

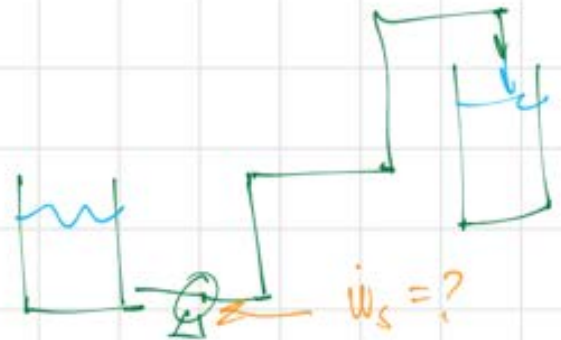
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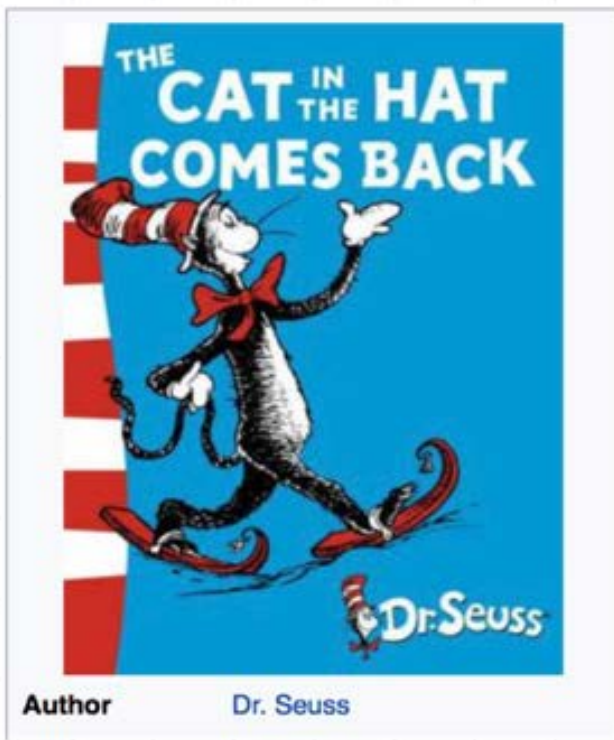
RECALL FROM LAST WEEK...



WHAT IS
 v_2 ?



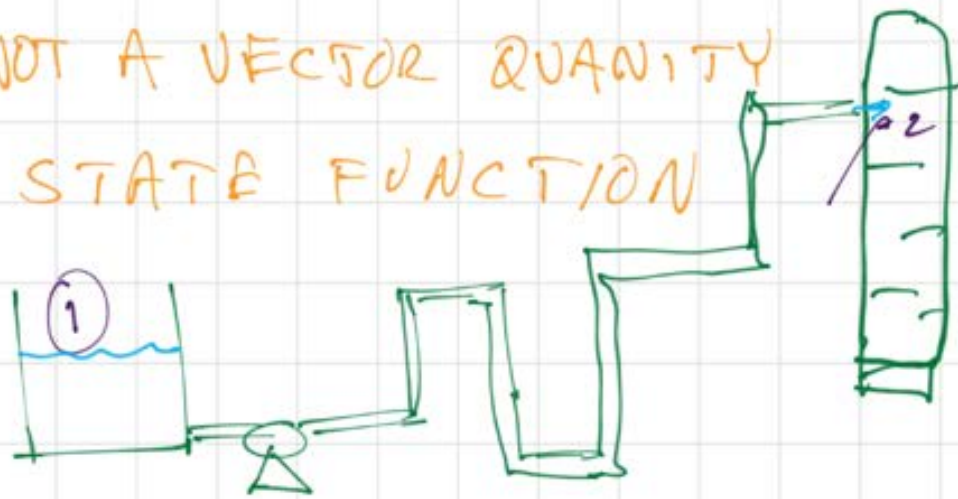
MOMENTUM EQUATION
OF NO USE ...



WE NEED
CAT'S !!

• NOT A VECTOR QUANTITY

• STATE FUNCTION



COULD CONSIDER CHANGE
FROM STATE ① → ②

FOR PIPE FLOW

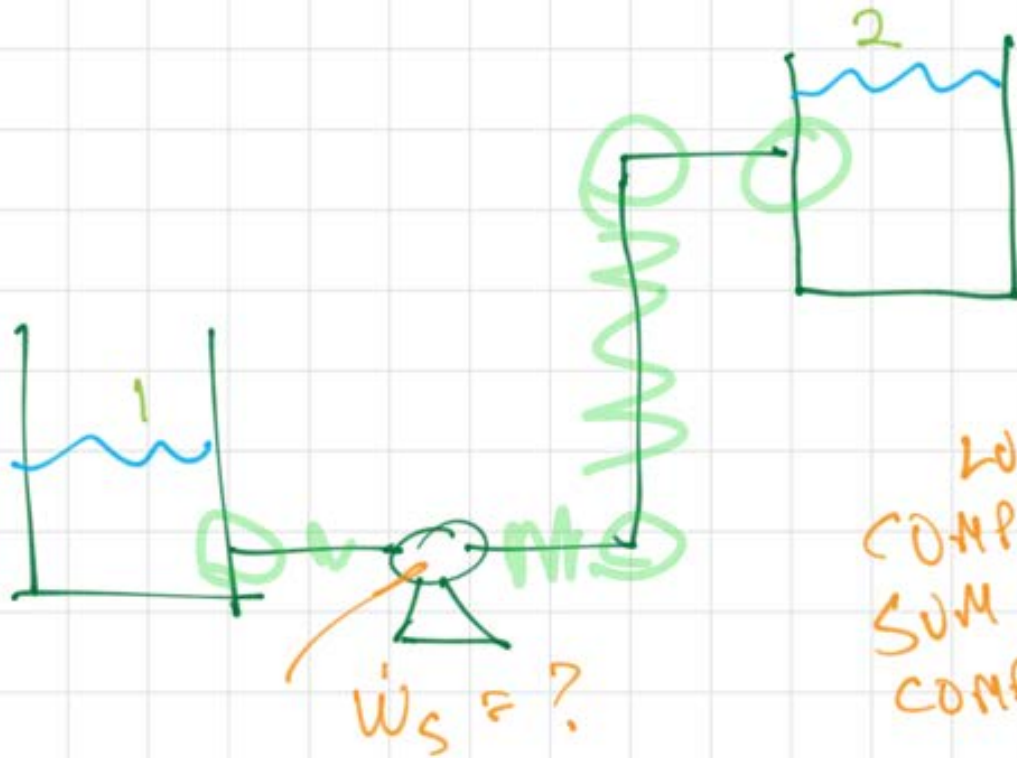
$$h_v = \frac{2 L f V^2}{D}$$

MORE GENERALLY ...

$$h_v = \frac{1}{2} K V^2 \quad \text{TABLES}$$

FOR MULTIPLE FITTINGS AND
PIPE SEGMENTS ...

$$h_v = \sum_i \frac{1}{2} K_i V_i^2$$

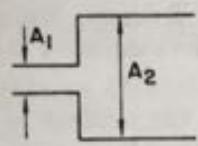
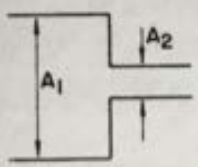


$$(gh_2 - gh_1) = \dot{W}_s - \sum_i l_{v_i}$$

$$\dot{W}_s = \dot{m}g(h_2 - h_1) + \dot{m} \sum_i l_{v_i}$$

$$\sum_i l_{v_i} = 2 \text{ ELBOWS} + 1 \text{ EXIT} \\ + 1 \text{ ENTRANCE} + \\ 4 \text{ STRAIGHT} \\ \text{PIECES OF} \\ \text{PIPE} \dots$$

TABLE 5-1
LOSSES IN FITTINGS AND VALVES FOR TURBULENT FLOW*

Fitting or valve	Velocity heads lost, K_f
90° elbow, standard	0.75
90° elbow, square	1.3
Coupling	0.04
Gate valve	
Open	0.17
Half-open	4.5
Globe valve, bevel seat	
Open	6.4
Half-open	9.5
Sudden expansion	$\left(\frac{A_2}{A_1} - 1\right)^2$
	
Sudden contraction	$\left(\frac{2}{m} - \frac{A_2}{A_1} - 1\right)^2$
	
	m is the root of the quadratic $\frac{1 - m(A_2/A_1)}{1 - (A_2/A_1)^2} = \left(\frac{m}{1.2}\right)^2$
Rounded entrance	0.05

*The result for the sudden expansion is derived in Sec. 6.2. The result for the sudden contraction is from Martin, *Chem. Eng. Educ.*, Summer 1974, p. 138. Other values are from *Perry's Handbook*.

Example 5.7

A liquid is pumped through a 50-mm-diameter smooth pipe between two tanks at a rate of 3 kg/s in the section of the process stream shown in Fig. 5-5. The liquid has properties $\rho = 10^3 \text{ kg/m}^3$, $\eta = 10^{-3} \text{ Pa}\cdot\text{s}$. The pressure above the

$$\Delta P = \frac{1}{2} \rho K V^2$$

↑
DOWNSTREAM
VELOCITY