

CBE 40445

8/21/20

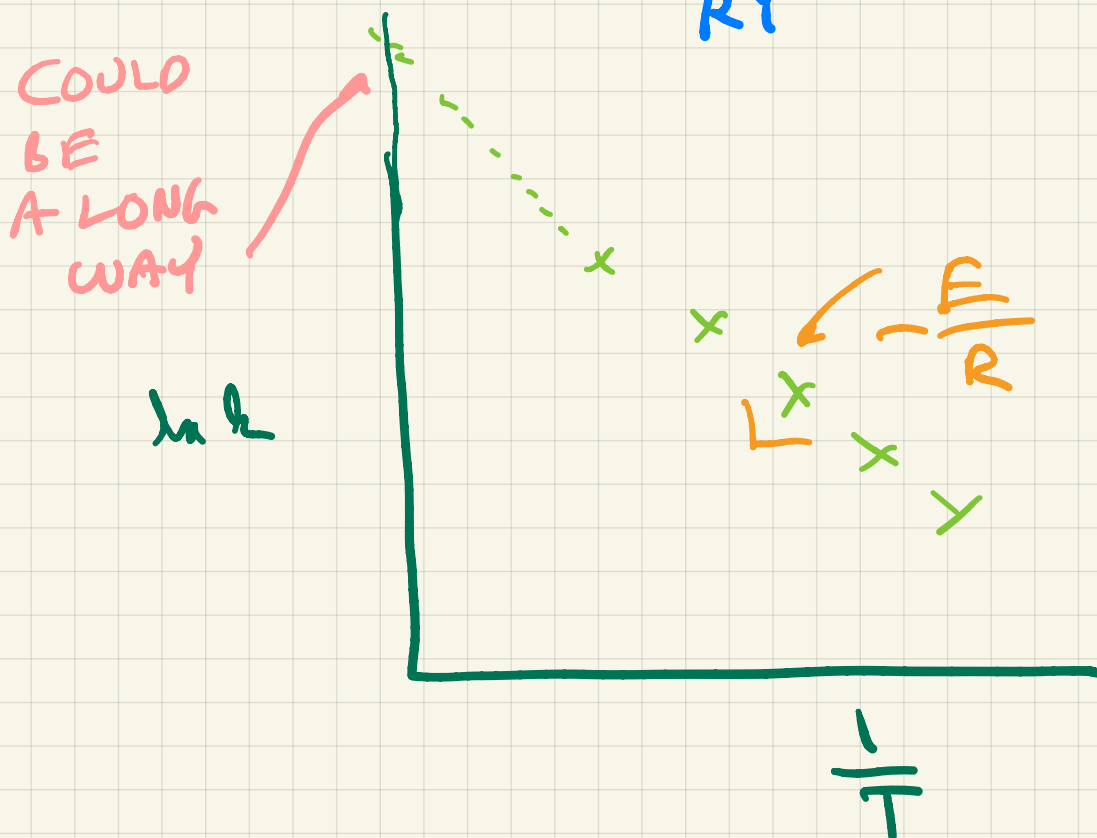
- DATA ANALYSIS
 - NOISY DATA
- 'FUNDAMENTAL' ASPECTS OF CHEMICAL KINETICS
 - TRANSITION STATE THEORY
- CHAPT - 3
 - CHEMICAL REACTORS

$$k = A \exp\left(-\frac{E}{RT}\right)$$

$$\frac{k}{A} = \exp\left(-\frac{E}{RT}\right)$$

$$\ln\left(\frac{k}{A}\right) = -\frac{E}{RT}$$

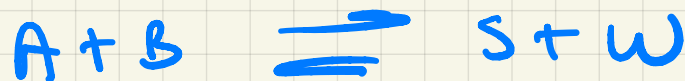
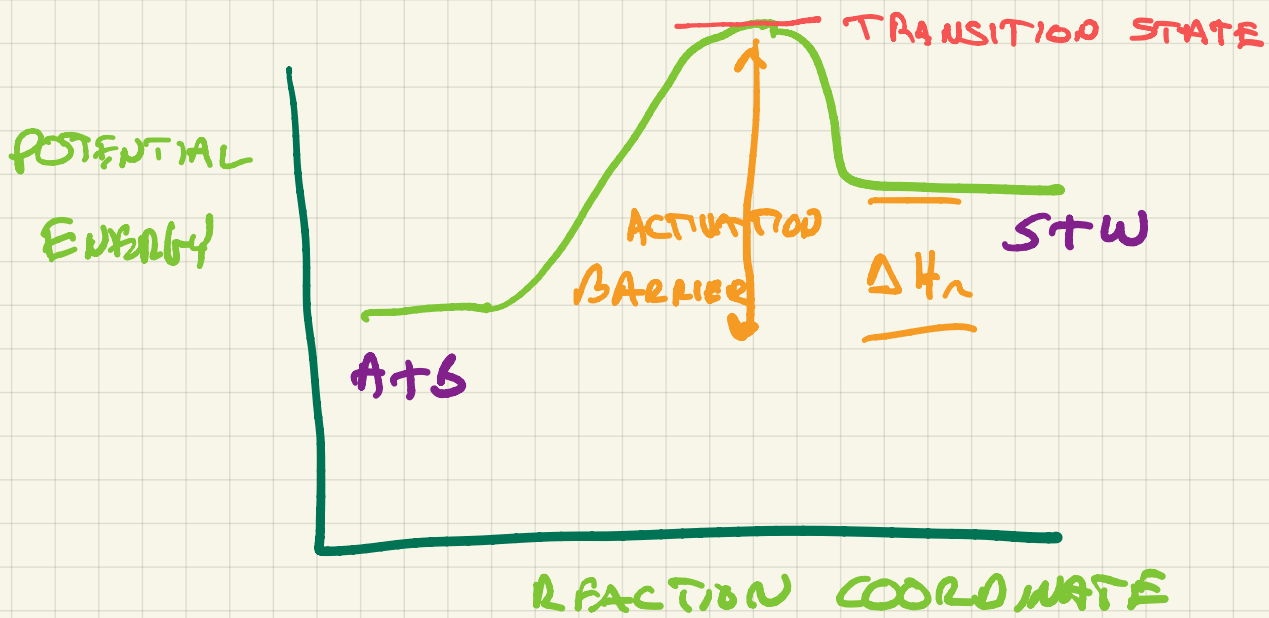
$$\ln k = -\frac{E}{RT} + \ln A$$



JUST GET A FROM E & k

PRESUMABLY THESE ARE BASED ON A NUMBER POINTS

II TRANSITION STATE THEORY¹



SO WE EXPECT THAT

AT EQUILIBRIUM

$$k_1 C_A C_B = k_2 C_S C_W$$

$$K_C = \frac{k_1}{k_2} = \frac{C_S C_W}{C_A C_B}$$

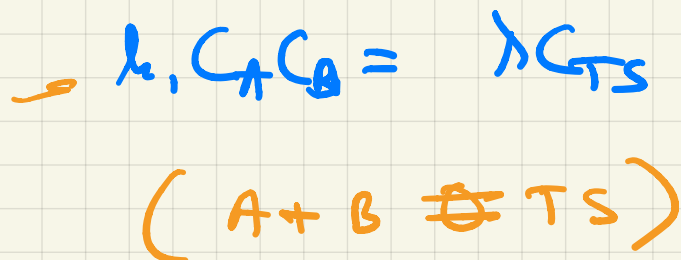
NOW INCLUDING

A TRANSITION STATE

$$: k_1 C_A C_B = k_2 C_S C_W = \lambda C_S$$

IF WE CONSIDER REACTANTS
GOING TO TRANSITION STATE:

RATE
OF
FORWARD
REACTION



WHICH GIVES...

$$K^\ddagger = \frac{C_{TS}}{C_A C_B}$$

(IF YOU
BELIEVE
THIS..)

THEN SOME THERMO:

ALL
FOR
A + B \rightleftharpoons TS

$$RT \ln K^\ddagger = -\Delta G_0^\ddagger = -\Delta H_0^\ddagger + T\Delta S_0^\ddagger$$

THUS

AGAIN
THERMO

$$C_{TS} = \exp\left[\frac{\Delta S_0^\ddagger}{R}\right] \exp\left[\frac{-\Delta H_0^\ddagger}{RT}\right] C_A C_B$$

SO THAT: $k_f C_A C_B = \lambda C_{TS}$

NOW A RATE

$$\lambda = k_f C_A C_B = \lambda \exp\left[\frac{\Delta S_0^\ddagger}{R}\right] \exp\left[\frac{-\Delta H_0^\ddagger}{RT}\right] C_A C_B$$

CONTINUING WITH

SOME ASSUMPTIONS OF

T. S.

BOLTZMAN CONSTANT

UNIVERSAL
FREQUENCY

$$\lambda = \frac{\bar{h}T}{h}$$

PLANK CONSTANT

WHICH GIVES !

GENERAL
RELATION!

$$\lambda = \left(\frac{\bar{h}T}{h} \right) \exp \left[\frac{\Delta S_0^\ddagger}{R} \right] \exp \left[\frac{-\Delta H_0^\ddagger}{RT} \right] C_A C_B$$

SO BACK TO ARRHENIUS...

$$\bar{A} = \left(\frac{\bar{h}T}{h} \right) \exp \left[\frac{\Delta S_0^\ddagger}{R} \right]$$

$$E = \Delta H_0^\ddagger$$

WE SEE LINEAR DEPENDENCE

ON T , BUT USUALLY

THIS IS SMALL COMPARED
TO EXPONENTIAL

$$S = k \log W$$



LVDWIG
BOLTZMANN
1844 - 1906

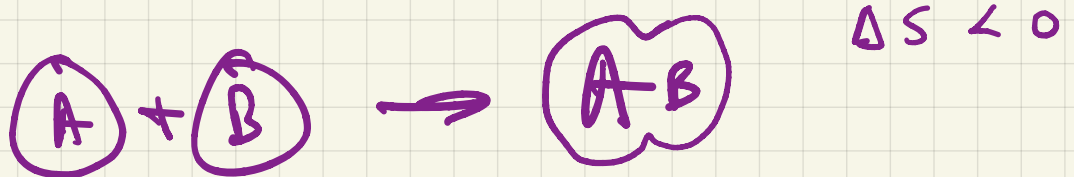
DR PHIL PAULA
BOLTZMANN
GRB. CHIASI
1893 - 1977
ARTHUR
BOLTZMANN

$$\bar{A} = \left(\frac{kT}{h} \right) \exp \left[\frac{\Delta S_0^\ddagger}{R} \right]$$

SO ΔS_0^\ddagger $A + B \rightarrow TS$

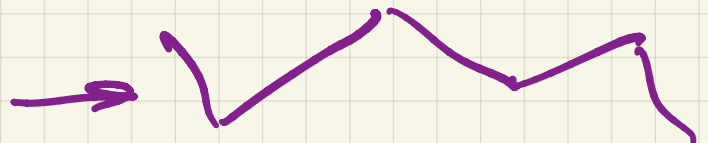
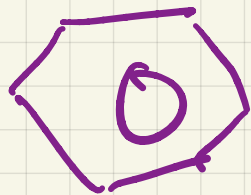
EXPECT MOLECULAR CONFIGURATION
TO BE IMPORTANT

AS ΔS_0 \uparrow A \uparrow



$$\Delta S \sim \left(\frac{10 \text{ J}}{\text{MOLE K}} \right)$$

$$R = \frac{8.314 \text{ J}}{\text{MOLE K}}$$



$$\exp \left[\frac{\Delta S_0^\ddagger}{R} \right] \text{ COULD BE } O(1)$$

OR MAYBE

$$.1 \leq \exp \left[\frac{\Delta S_0^\ddagger}{R} \right] \leq 10$$

THUS AS A BASELINE!

$$\bar{A} \hat{=} \frac{\bar{hT}}{h} \hat{=} 10^{13} / s$$

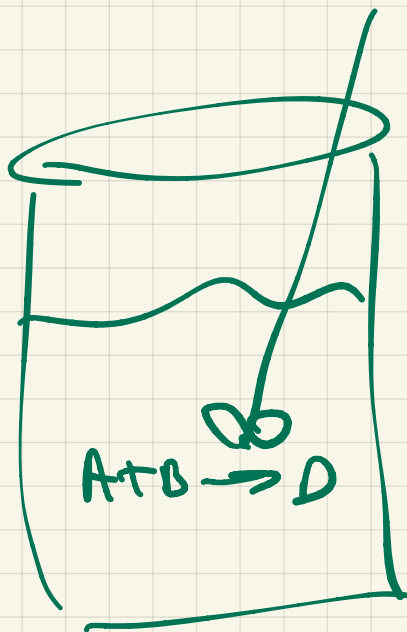
D & D NOTE THAT MOST
OF THE TIME ΔH_j^\ddagger , ΔS_j^\ddagger
ARE NOT REALLY KNOWN..

SO MOST OF THE TIME
WE USE ALLHEN IUC..

CHAPTER 3

HOW DO WE GET KINETIC
DATA?

IN A LAB, YOU USUALLY
USE A BATCH OR
SEMI-BATCH REACTOR



BATCH

FEED IN
B



SEMI BATCH

(MOLES)
MASS BALANCE

SPECIES
 i

RATE OF
CHANGE OF
MOLES OF
 i IN REACTOR

=

FLOW RATE
OF i
INTO
REACTOR

- FLOW
RATE
OF i
OUT OF
REACTOR

+

RATE AT
WHICH

i IS PRODUCED/CONSUMED

BY REACTION

THUS IN TERMS OF MOLES...

$$\frac{dn_i}{dt} = 0 - 0 + \nu_i r V$$

REACTION RATE
VOLUME

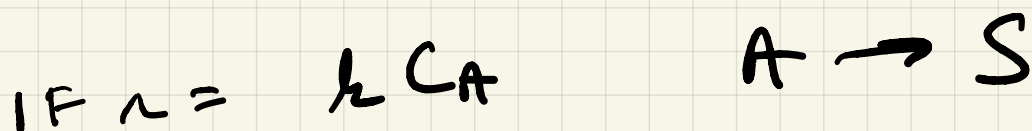
STOICHIOMETRIC
COEFFICIENT

VOLUME

GENERALLY AN INITIAL
VALUE PROBLEM

COULD ALSO WRITE

$$\frac{dV C_i}{dt} = \nu_i r V$$



$$\frac{dV C_A}{dt} = -k C_A V$$

IF $V = \text{CONST}$

~~$$V \frac{dC_A}{dt} = -k C_A V$$~~

COULD ALSO WRITE:

$$M_i^0 \frac{df_i}{dt} = -v_i \cdot V \quad f_i(t=0) = 0$$

SUPPOSE $A + B \rightarrow S$

$$r = k C_A C_B$$

$$C_{A0} \neq C_{B0}$$

$$dC_A = dC_B$$

$$C_{A0} - C_A = C_{B0} - C_B$$

$V = \text{CONST}$

$$\frac{dC_A}{dt} = -k C_A C_B$$

$$\frac{dC_A}{dt} = -k C_A (C_{B0} - C_{A0} + C_A)$$

$$\frac{dC_A}{C_A (C_A - (C_{A0} - C_{B0}))} = k dt$$

$$\frac{dC_A}{C_A (C_A - (C_{A0} - C_B))} = k dt$$

$$\ln \left(\frac{C_{A0} (C_A(t) - (C_{A0} - C_{B0}))}{C_{A0} - C_{B0}} \right) = kt$$