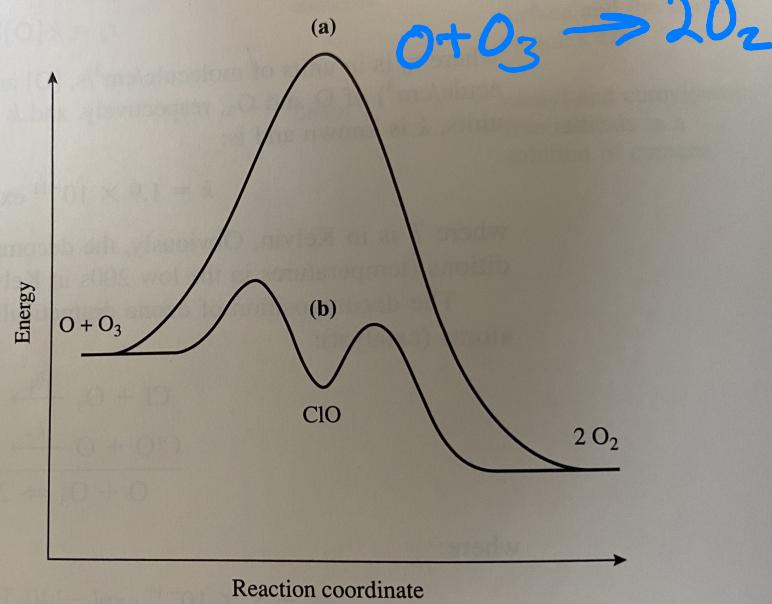


CBE 40445  
9/9/20

ANALYSIS OF COMPLEX REACTION  
SCHEMES . . .

# OZONE DECOMPOSITION

At  $T = 200\text{ K}$ ,  $k_c/k_d = 100$ . This means that the rate of decomposition of ozone is 100 times faster than the rate of formation of oxygen atoms by the direct reaction. The catalyst (Cl). As illustrated in the energy diagram shown in Figure 4.1.2, the addition of Cl to the catalyst lowers the activation barrier. The Cl catalyst first reacts with O to form ClO, which then reacts with O<sub>3</sub> to form O<sub>2</sub>.



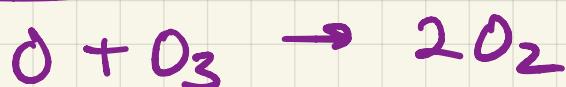
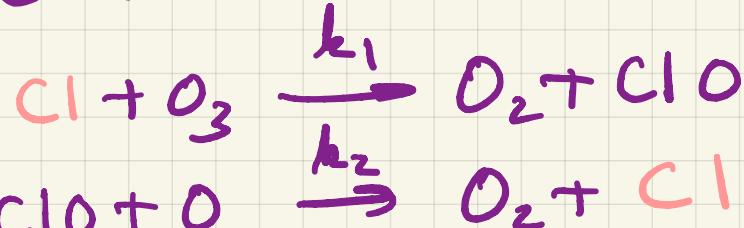
**Figure 4.1.2 |**  
Energy versus reaction coordinate for ozone decomposition.  
(a) direct reaction, (b) Cl catalyzed reaction.

$$k = k [O][O_3]$$

$$k = 1.9 \times 10^{-11} \exp\left(-\frac{2300}{T}\right)$$

"SLOW" !!

IF CHLORINE IS PRESENT . . .



$$k_1 = 5 \times 10^{-11} \exp\left(-\frac{140}{T}\right)$$

$$k_2 = 1.1 \times 10^{-10} \exp\left(-\frac{220}{T}\right)$$

$\frac{\text{cm}^3}{\text{s molecule}}$

CAN SHOW . . .

$$n_c = \frac{k_1 k_2 [O][O_3]([Cl] + [ClO])}{k_1 [O_3] + k_2 [O]}$$

BUT  $[O] \ll [O_3]$   $k_1 \approx k_2$

$$n_c = k_2 ([O][Cl] + [ClO])$$

CATALYZED  
DIRECT

$$\frac{n_c}{n_d} = \frac{k_2 ([Cl] + [ClO])}{k_3 [O_3]}$$

ALSO

$$\frac{[Cl] + [ClO]}{[O_3]} \sim 10^{-3}$$

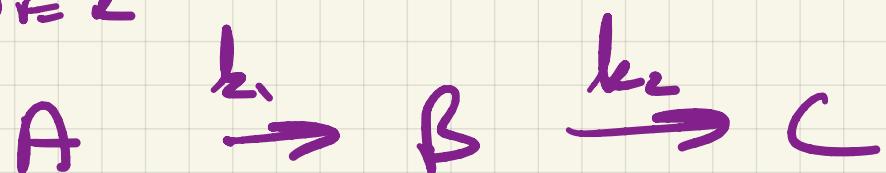
$$\frac{n_c}{n_d} = \frac{k_2}{k} \times 10^{-3} = 6 \times 10^{-3} \exp\left(\frac{-2050}{T}\right)$$

@ T = 200 K,  $\frac{n_c}{n_d} = 200$

# FINALLY ... THE REAL NAME OF THE CHAPTER - - .

## THE STEADY-STATE APPROXIMATION

CONSIDER



$$C_A(t=0) = C_{A0}, \quad C_{B0} = 0, \quad C_{C0} = 0$$

$$x = \frac{C_A}{C_{A0}}$$

$$y = \frac{C_B}{C_{A0}}$$

$$\frac{dx}{dt} = -k_1 x$$

$$\frac{dy}{dt} = k_1 x - k_2 y$$

$$w = \frac{C_C}{C_{A0}}$$

$$\frac{dw}{dt} = k_2 y$$

$C_A^0$  denotes the concentration of A at time zero. The three differential equations for this system are:

$$\frac{dx}{dt} = -k_1 x \quad \frac{dy}{dt} = k_1 x - k_2 y \quad \frac{dw}{dt} = k_2 y \quad (4.2.1)$$

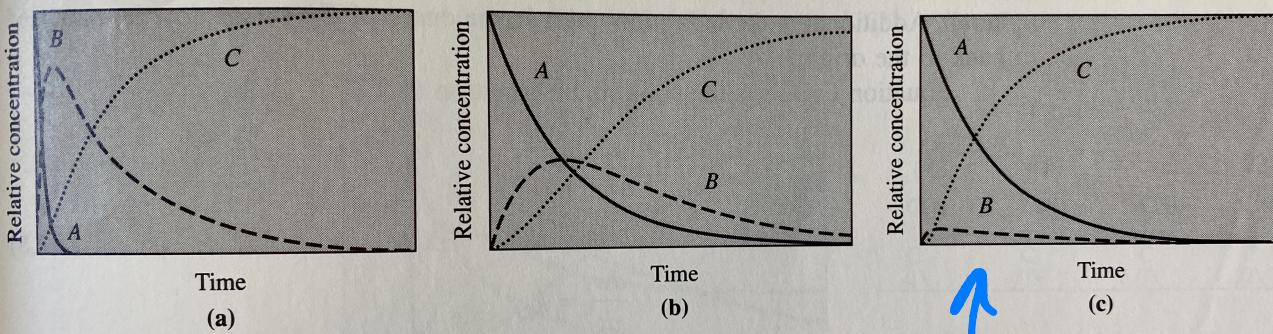
where  $x = C_A/C_A^0$ ,  $y = C_B/C_A^0$ , and  $w = C_C/C_A^0$ . Integration of Equation (4.2.1) with  $x = 1$ ,  $y = 0$ ,  $w = 0$  at  $t = 0$  gives:

$$\left. \begin{aligned} x &= \exp(-k_1 t) \\ y &= \frac{k_1}{k_2 - k_1} [\exp(-k_1 t) - \exp(-k_2 t)] \\ w &= 1 - \frac{k_2}{k_2 - k_1} \exp(-k_1 t) + \frac{k_1}{k_2 - k_1} \exp(-k_2 t) \end{aligned} \right\} \quad (4.2.2)$$

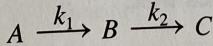
## BEING GOOD CHEMICAL ENGINEERS WE PLOT THE RESULT

CHAPTER 4 The Steady-State Approximation: Catalysis

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**Figure 4.2.1 |**  
Two first-order reactions in series.



(a)  $k_2 = 0.1 k_1$ , (b)  $k_2 = k_1$ , (c)  $k_2 = 10 k_1$ .

↑ THIS LOOKS  
INTERESTING

NOT MUCH B, AND DOESN'T CHANGE..

( $k_2 \gg k_1$ )

$$x = \exp(-k_1 t)$$

$$y = \frac{k_1}{k_2} \exp(-k_2 t)$$

$$w = 1 - \exp(-k_1 t)$$

THIS IS THE SOLUTION TO!

$$\frac{dx}{dt} = -k_1 x$$

$$0 = k_1 x - k_2 y$$

$$\frac{dw}{dt} = k_2 y$$

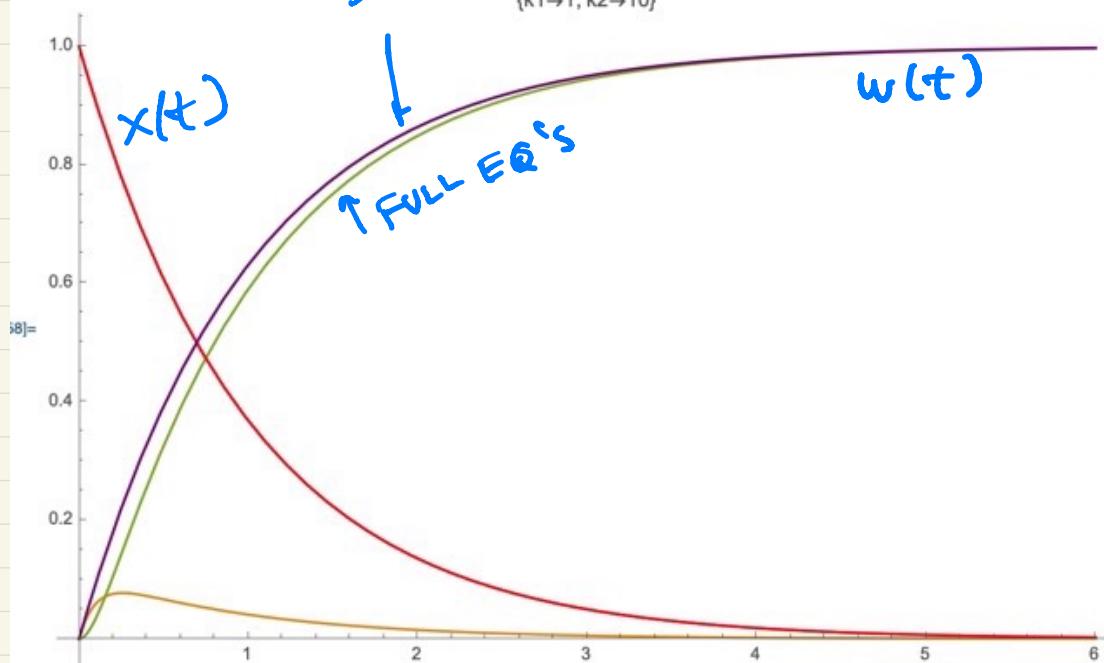
THUS WE PRESUME:

$$\frac{dy}{dt} = 0 \quad \text{"STEADY-STATE" ASSUMPTION.}$$

WE WILL USE ("TRYOUT") THIS SIMPLIFICATION FOR REACTION INTERMEDIATES ...

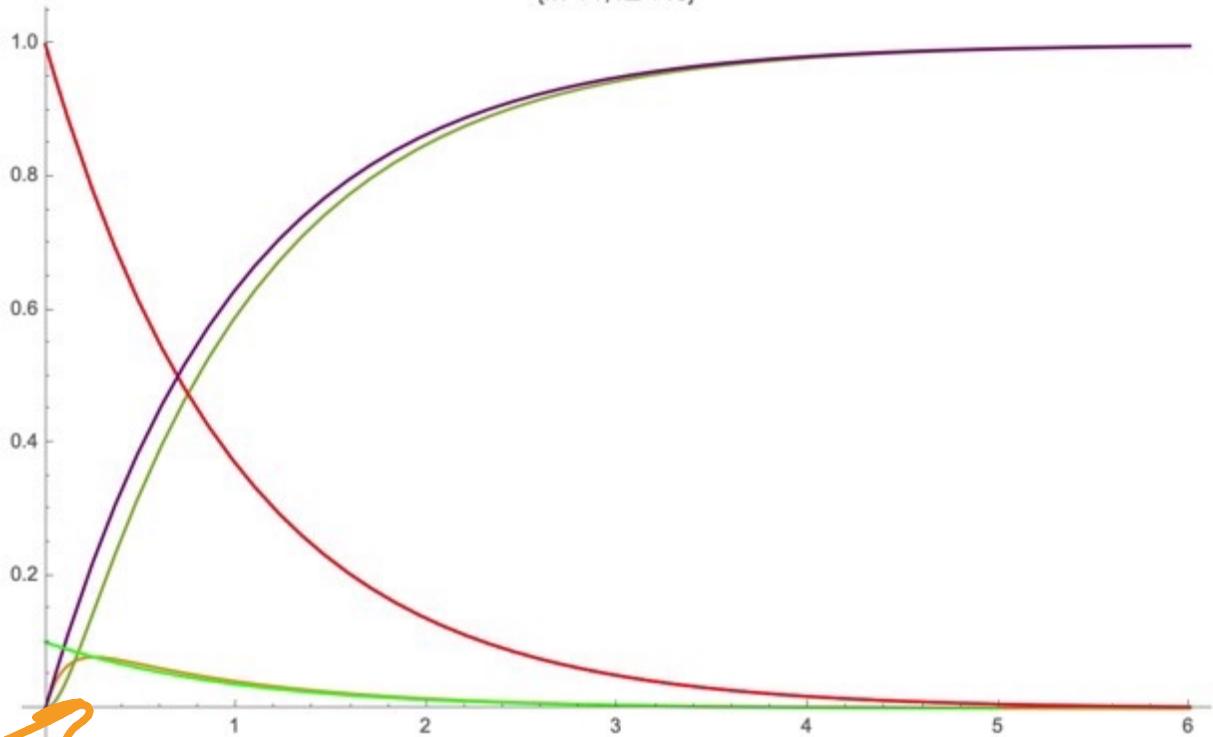
STEADY-STATE APPROXIMATION

$\{k_1 \rightarrow 1, k_2 \rightarrow 10\}$



Show[%358, %]

$\{k_1 \rightarrow 1, k_2 \rightarrow 10\}$



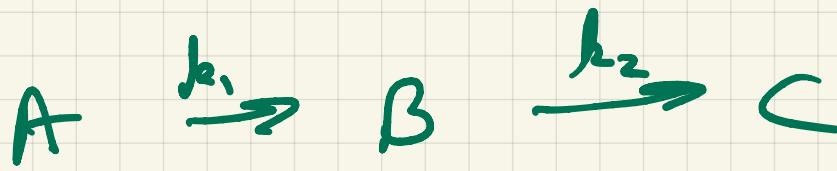
IF WE INCLUDE  $y(t) = \frac{k_1}{k_2} \exp(-k_1 t)$

CONCLUSION : IF THIS  
"ASSUMPTION" HELPS TO  
SIMPLIFY AND "ELUCIDATE"  
COMPLEX MECHANISMS . . .

GO AHEAD & TRY ! !

CAVEAT : THERE IS AN  
INDUCTION TIME : "RELAXATION TIME"  
WHILE THIS APPROXIMATION DOESN'T  
WORK BECAUSE THE CONCENTRATION  
IS BUILDING UP TO THE  
STEADY - STATE

LET'S TAKE A QUICK LOOK:



WE WANT TO CONSIDER THIS REACTION

$$\text{WITH } \frac{dC_B}{dt} = 0, \quad k_2 \gg k_1$$

STEADY STATE CONCENTRATION

FIRST ALLOW THAT  $C_B$  IS NOT AT  $C_B^*$

$$C_B = C_B^*(1 + \bar{\epsilon})$$

THIS

$$\frac{dC_B}{dt} = C_B^* \frac{d\bar{\epsilon}}{dt} + (1 + \bar{\epsilon}) \frac{dC_B^*}{dt}$$

FROM REACTION MECHANISM

$$\frac{dC_B}{dt} = +k_1 C_A - k_2 C_B$$

FROM PREVIOUS ANALYSIS THE STEADY STATE OF  $C_B$

$$C_B^* = \frac{k_1}{k_2} C_A$$

$$\Rightarrow \frac{dC_B^*}{dt} = \frac{k_1}{k_2} \frac{dC_A}{dt} = -\frac{k_1^2}{k_2} C_A$$

USING  $\frac{dC_A}{dt} = -k_1 C_A$

$$\frac{dC_B}{dt} = +k_1 C_A - k_2 C_B$$

NOW FROM ABOVE:

$$\frac{dC_B}{dt} = C_B^* \frac{d\bar{\epsilon}}{dt} + (1+\bar{\epsilon}) \frac{dC_B^*}{dt}$$

$$C_B^* \frac{d\bar{\epsilon}}{dt} + (1+\bar{\epsilon}) \frac{dC_B^*}{dt} = k_1 C_A - k_2 C_B$$

$$\frac{k_1 C_A}{k_2} \frac{d\bar{\epsilon}}{dt} + (1+\bar{\epsilon}) \left( -\frac{k_1^2}{k_2} C_A \right) = k_1 C_A - k_2 C_B$$

$$\Rightarrow \frac{d\bar{\epsilon}}{dt} + (k_2 - k_1) \bar{\epsilon} - k_1 = 0$$

$$\boxed{\begin{array}{l} \bar{\epsilon} = -1 \\ C_B = 0 \\ t = 0 \end{array}}$$

$$k_1 c_a - k_2 c_b = c_{bs}[t] \times D[\epsilon[t], t] + (1 + \epsilon) D[c_{bs}[t], t]$$

$$c_a k_1 - c_b k_2 = (1 + \epsilon) c_{bs}'[t] + c_{bs}[t] \epsilon'[t]$$

$$\%/. D[c_{bs}[t], t] \rightarrow -k_1^2 / k_2 c_a[t]$$

$$c_a[t] k_1 - c_b[t] k_2 = -\frac{k_1^2 (1 + \epsilon[t]) c_a[t]}{k_2} + c_{bs}[t] \epsilon'[t]$$

$$k_1 c_a[t] - k_2 c_b[t] = -\frac{k_1^2 c_a[t] (1 + \epsilon[t])}{k_2} + c_{bs}[t] \epsilon'[t]$$

$$\%/. c_{bs}[t] \rightarrow k_1 / k_2 c_a[t]$$

$$k_1 c_a[t] - k_2 c_b[t] = -\frac{k_1^2 c_a[t] (1 + \epsilon[t])}{k_2} + \frac{k_1 c_a[t] \epsilon'[t]}{k_2}$$

$$\%/. c_b[t] \rightarrow k_1 / k_2 c_a[t] (1 + \epsilon[t])$$

$$k_1 c_a[t] - k_1 c_a[t] (1 + \epsilon[t]) = -\frac{k_1^2 c_a[t] (1 + \epsilon[t])}{k_2} + \frac{k_1 c_a[t] \epsilon'[t]}{k_2}$$

Solve[% ,  $\epsilon'[t]]$

$$\{\{\epsilon'[t] \rightarrow k_1 + k_1 \epsilon[t] - k_2 \epsilon[t]\}\}$$

$$\bar{\varepsilon} = - \frac{1}{K-1} \left\{ \bar{K} - \exp((\bar{K}-1)k_2 t) \right\}$$

$$K \equiv k_1/k_2 < 1$$

AT SUFFICIENTLY LARGE TIME:

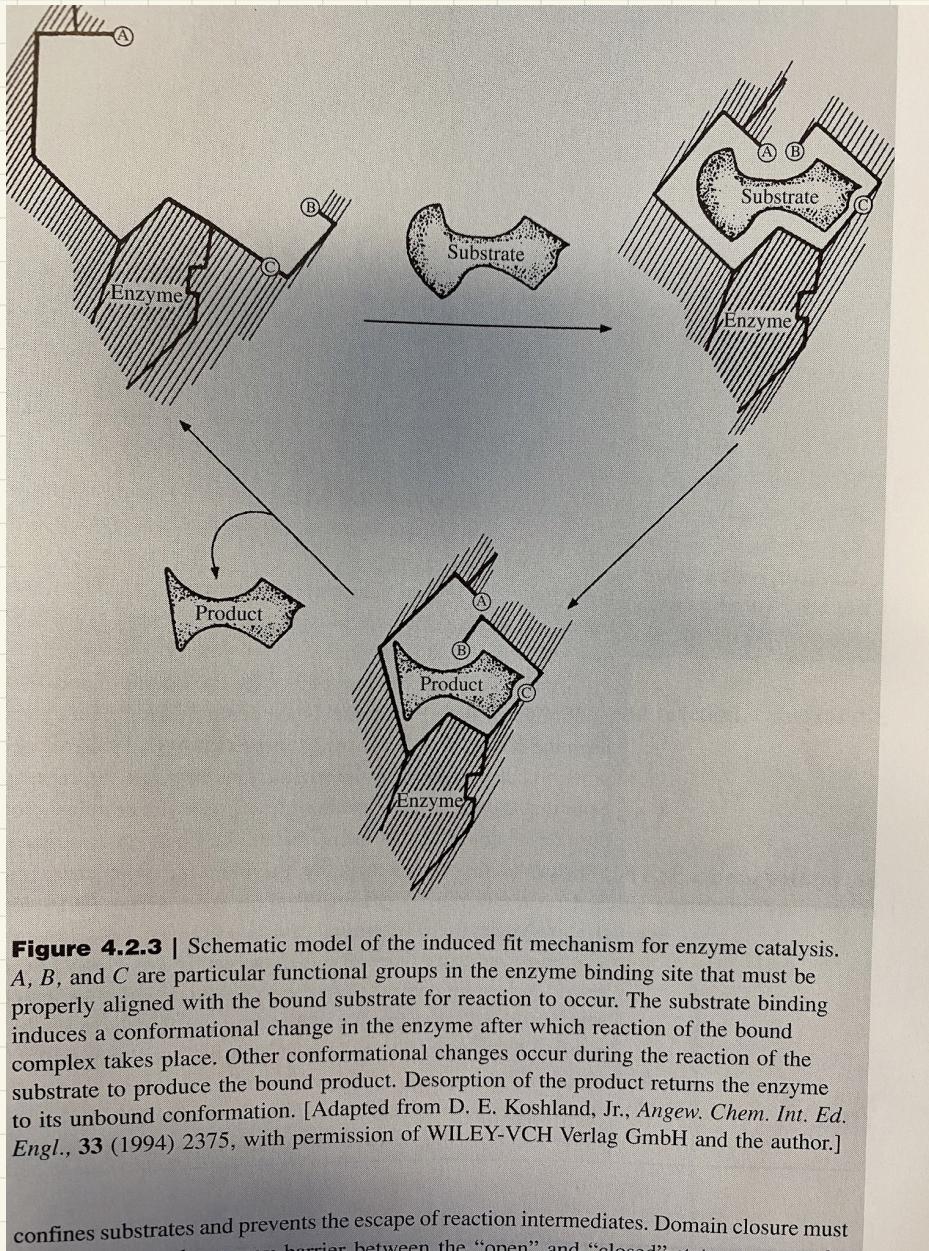
$$\bar{\varepsilon} = \bar{K} .$$

THIS TIME IS OBTAINED FROM:

$$\exp(-k_2 t) \sim \exp(-4)$$

$$t \approx \frac{4}{k_2}$$

# EXAMPLE OF ENZYME CATALYSIS



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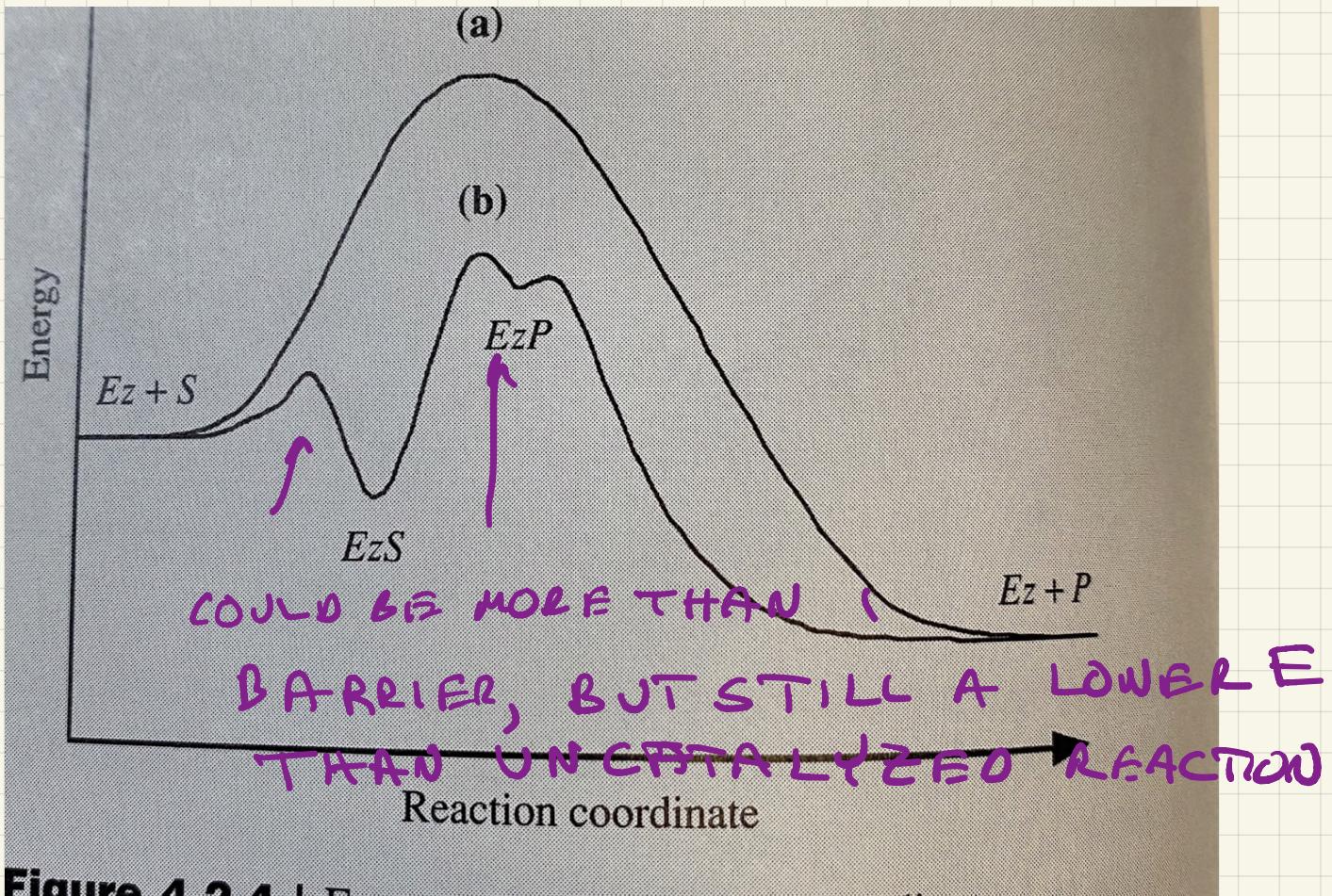
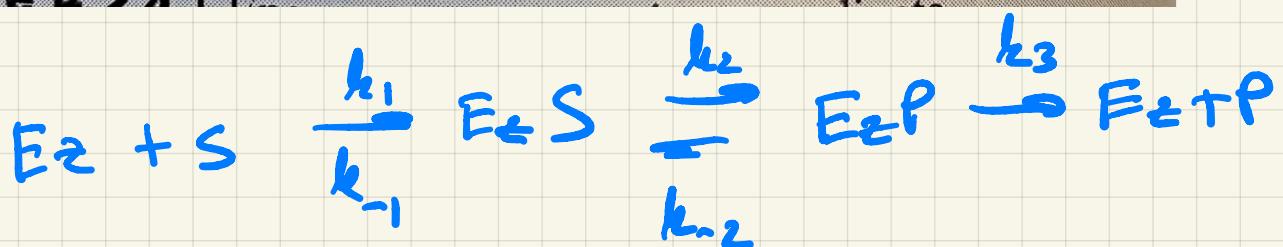


Figure 4.2.4 | Energy profile diagram for a reaction catalyzed by  $E_2$ .



$$\frac{dC_S}{dt} = -k_1 C_{E_2} C_S + k_{-1} C_{E_2S}$$

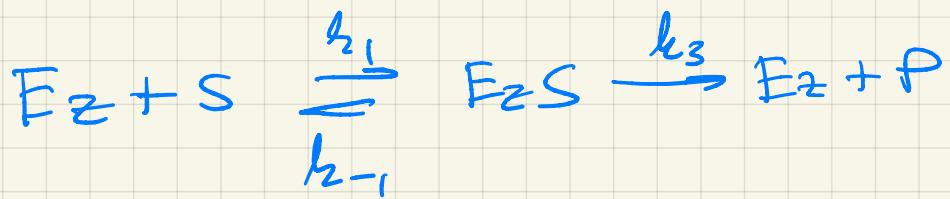
$$\frac{dC_{E_2S}}{dt} = k_1 C_{E_2} C_S - k_{-1} C_{E_2S} - k_2 C_{E_2S} + k_{-2} C_{E_2P}$$

$$\frac{dC_{E_2P}}{dt} = k_2 C_{E_2S} - k_{-2} C_{E_2P} - k_3 C_{E_2P}$$

$$\frac{dC_P}{dt} = k_3 C_{E_2P}$$

BUT MANY CASES ARE SUCH

THAT  $k_3 \gg k_2 + k_{-1}$



$$\frac{dC_s}{dt} = -k_1 C_s C_{Ez} + k_{-1} C_{EzS}$$

$$\frac{dC_{EzS}}{dt} = k_1 C_s C_{Ez} - k_{-1} C_{EzS} - k_3 C_{EzS}$$

$$\frac{dC_p}{dt} = k_3 C_{EzS}$$

$$C_E^o = C_{Ez} + C_{EzS}$$

$$\frac{dC_{EzS}}{dt} = 0 = k_1 C_s C_{Ez} - k_{-1} C_{EzS} - k_3 C_{EzS}$$

$$C_{EzS} = \frac{k_1 C_s C_{Ez}}{k_{-1} + k_3} = \frac{C_s C_{Ez}}{K_m}$$

$$K_m = \frac{k_{-1} + k_3}{k_1}$$

PART OF  
RATIONALE!  
WE CAN'T GET  
ALL CONSTANTS  
ANYWAY!

$$C_{E2}^{\circ} = C_{E2} + C_{E2S}$$

$$C_{E2S} = \frac{C_S C_{E2}}{K_m}$$

$$C_{E2S} = \frac{C_{E2}^{\circ} C_S - C_{E2S} C_S}{K_m}$$

SOLVE

$$C_{E2S} = \frac{C_{E2}^{\circ} C_S}{K_m + C_S}$$

WITKST GIVES . . .

$$\frac{dC_P}{dt} = \frac{k_3 C_{E2}^{\circ} C_S}{K_m + C_S}$$

OR

$$\frac{dC_P}{dt} = - \frac{dC_S}{dt} = \frac{\lambda_{MAX} C_S}{K_m + C_S}$$

$$\lambda_{MAX} = k_3 C_{E2}^{\circ}$$

↗

STANDARD  
FORM