

A SUMMER OVERSEAS EXPERIENCE
AT THE IMPERIAL COLLEGE CO₂
CAPTURE PILOT PLANT

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THE CHALLENGE

- While the University is very keen on overseas study and some of the other Engineering departments had in-semester programs,
 - The previous department chair (i.e., me) was not enthralled with the ND template:
 - ND courses taught by ND faculty — or people hired to teach a specific course — taught in the ND building in country X.
- The incoming chair (ejm) found out that Imperial College had just built a new fully-instrumented CO₂ capture (into MEA) pilot plant and that they were offering summer session courses utilizing it. This could be paired with a standard CHE undergraduate lab course (they have a very extensive lab).
 - So he signed us up!

THE CHALLENGE

- So we recruited a group of students — who were all just finishing Sophomore year. Ideally, the Pilot Plant course would be a Senior elective and the lab is 2nd semester Junior year for us.....
 - It is obvious now, but at the time we didn't realize they would all be this “young”.
- For the first time, I had no contact with the students or any aspect of the planned courses before going ... One of our teaching faculty was going with them.
- However, in the first morning orientation session, within 15 minutes, I knew that we needed to have a plan for how to prepare the students for next year, to be able to maximize their learning in the Pilot Plant and to be able to run experiments and write lab reports.

MORE CHALLENGE

- Students “claim” to spend ~10+ hours per week outside of class for the undergraduate laboratory course taught on campus
- This is above a “safe” number for a lecture course to successfully translate to the 6 week, “distracting” location
 - e.g. “Mechanics” for Sophomore ME’s didn’t work at all.
- So we needed to devise a schedule of lab sessions, work periods and due dates to make the course work.
 - We also needed “on-call” faculty consulting to increase the efficiency of student effort.

IMPERIAL COLLEGE IS IN A REALLY NICE LOCATION!



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THE STRATEGY

- Provide the maximal alignment between laboratory experiments and fundamental topics that govern the Pilot Plant processes.
- Conduct a semester long, one hour per week, series of lectures on these fundamental topics, but with continual threading of the pilot plant operations as examples.
 - We are limited in the amount of outside work — or its intensity, because students are taking *thermodynamics*, “*num-stats*”, *Orgo II* and many also *linear algebra/differential equations*.
- We start each class with the CO₂-MEA process diagram, review various operational aspects and then focus on a specific operation.

FUNDAMENTAL TOPICS: *UNIT OPERATIONS*

- Thermodynamics (energy/mass conservation)
 - We can trust the in-semester course to cover this.
- Fluid flow
- Heat transfer
- Mass transfer/gas absorption
- Process control

PROCESS DIAGRAM

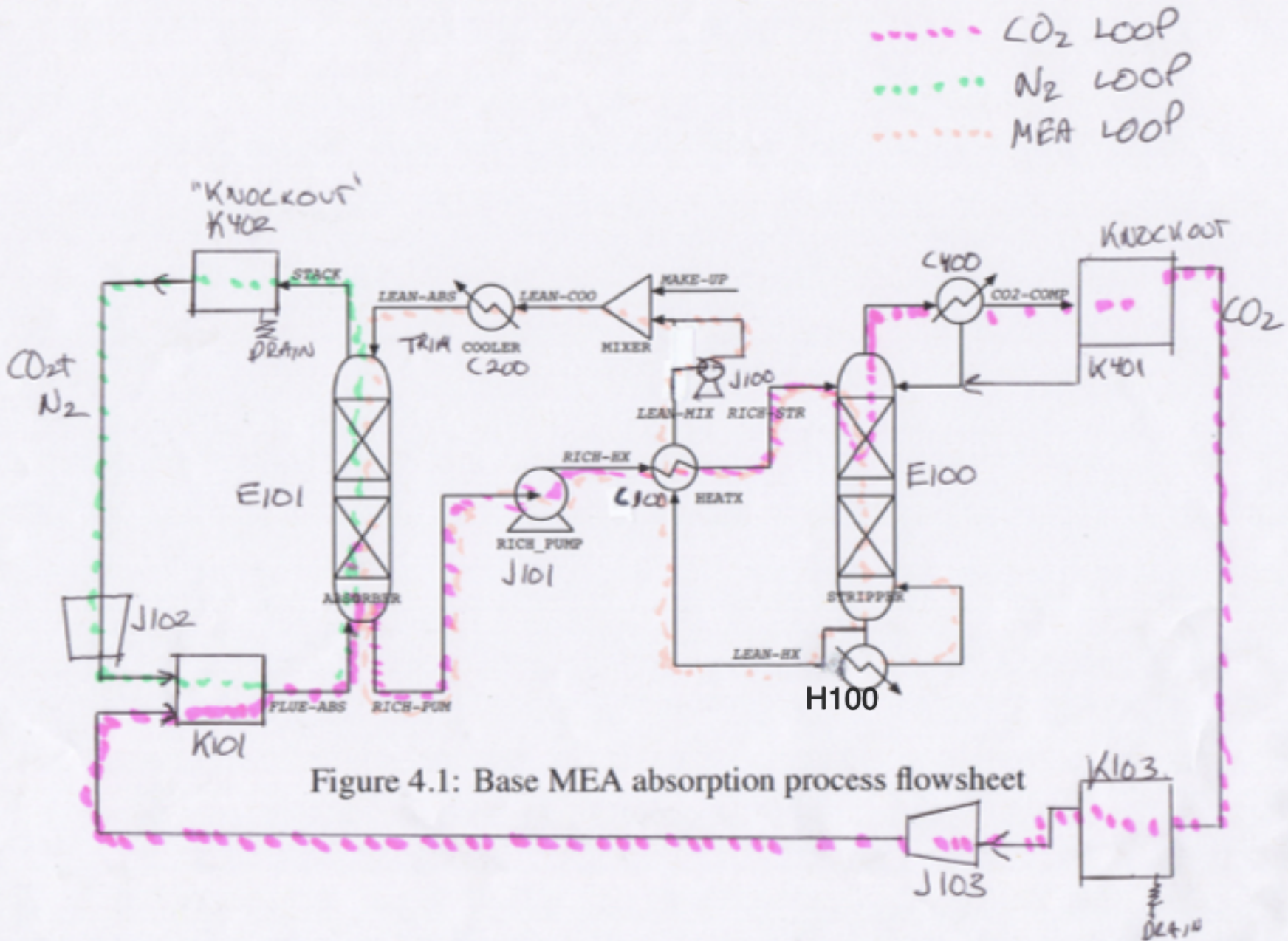
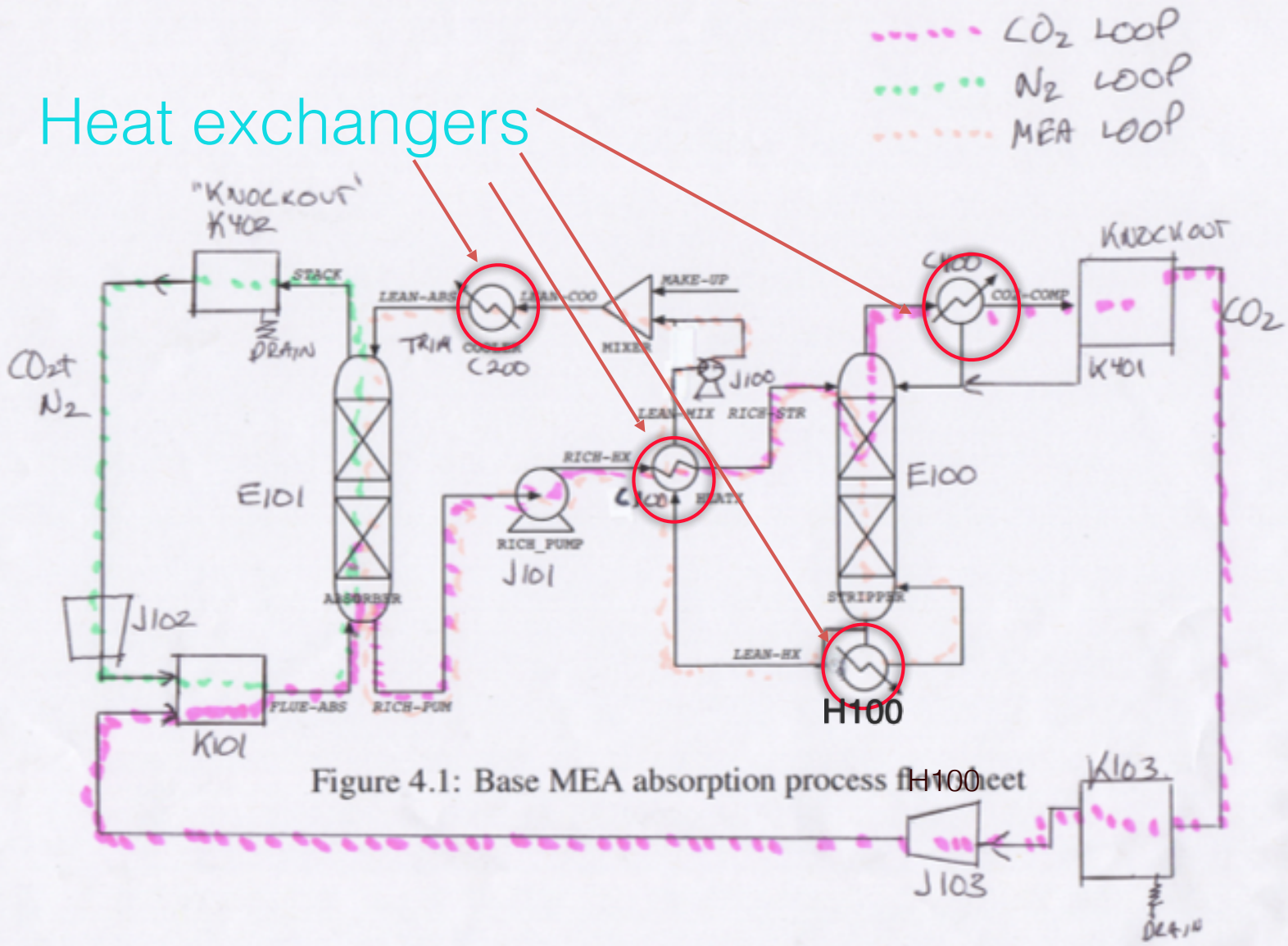


Figure 4.1: Base MEA absorption process flowsheet

IMPERIAL FLOWSHEET

Heat exchangers



EXAMPLE TOPIC: HEAT EXCHANGE IN MEA PROCESS

- Students need to calculate heat loads on the various heat exchangers.
 - Check efficiencies and *effectiveness*
 - One of the plate heat exchangers would be better with more plates—the other has plenty
- They also get overall heat transfer coefficients and compare to predictions from correlations.

IMPERIAL HEAT EXCHANGERS

C200



H100



HEAT TRANSFER LAB EXPERIMENT

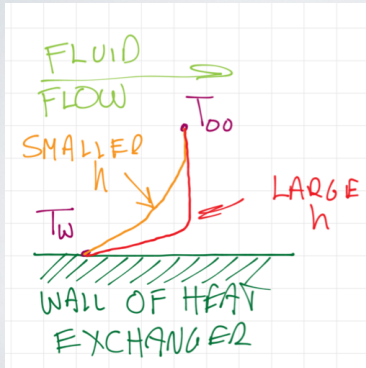


LAB HEAT TRANSFER EXPERIMENT

- Efficiencies, and effectiveness and heat transfer coefficients and comparisons for shell and tube, plate, double-pipe and air-water exchangers.
 - The log-mean temperature driving force is discussed in the lectures
 - The logarithmic driving force also arises in the gas absorption experiment.
 - Cocurrent versus Countercurrent for the double-pipe heat exchanger
 - One data set to try to match with standard Nusselt number correlations.

SOME EXAMPLE LECTURE SLIDES

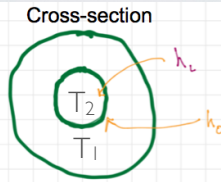
WALL REGION OF HEAT EXCHANGER: "FORCED CONVECTION"



Steeper gradient is associated with faster heat transfer

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HEAT EXCHANGER



Heat transfer resistance occurs at both inside and outside of inner pipe, hence there is a heat transfer coefficient for each side.

Sum of resistances used to get an overall heat transfer coefficient, U

$$U_i \equiv \frac{q}{A_i \Delta T} \quad \Delta T = T_2 - T_1$$

$$\frac{1}{A_i U_i} = \frac{1}{h_i A_i} + \frac{1}{k A} + \frac{1}{h_o A_o}$$

inside resistance outside resistance

$$\frac{1}{U_i} = \frac{1}{h_i} + \frac{A_i}{k A} + \frac{A_i}{h_o A_i}$$

resistance associated with pipe wall

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The resistance of the pipe wall will usually be much smaller than the contributions from the heat transfer coefficients if the pipe is made of a metal, but if we want to be precise we should write it as

$$\frac{A_i \ln \frac{d_{\text{out}}}{d_{\text{in}}}}{2 \pi L}$$

Note that all of the areas are $\pi d L$ for a specified L .

A U BASED ON THE OUTSIDE OF THE (INNER) PIPE IS:

$$U_o \equiv \frac{q}{A_o \Delta T}$$

$$\frac{1}{U_o} = \frac{A_o}{A_i h_i} + \frac{A_o \ln \frac{d_o}{d_i}}{2 \pi L k} + \frac{1}{h_o}$$

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DIFFERENTIAL ANALYSIS TO GET LENGTH OF HEAT EXCHANGER

- The steam keeps the pipe wall at a constant temperature, but the temperature of the water in the pipe is changing. We will need a differential formulation of the temperature change along the pipe and then need to integrate to get the answer.



- Consider a differential slice of pipe.

STEADY STATE, DIFFERENTIAL SLICE OF PIPE

CHANGE IN ENTHALPY OF FLUID = RATE OF HEAT CROSSING PIPE WALL

$$\dot{m}(h_{\text{out}} - h_{\text{in}}) = q$$

$$\dot{m} c_p (T_{\text{out}} - T_{\text{in}}) = -h \pi D L (T - T_{\text{wall}})$$

SHRINK TO Δz

$$\dot{m} c_p \Delta T = h \pi D \Delta z (T - T_{\text{wall}})$$

$$\frac{\Delta T}{\Delta z} = -\frac{h \pi D}{\dot{m} c_p} (T - T_{\text{wall}})$$

Newton's Law of cooling

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$$\Delta z \rightarrow 0$$

$$\frac{dT}{dz} = -\frac{h \pi D}{\dot{m} c_p} (T - T_{\text{wall}})$$

NOW INTEGRATE FROM T = 25C TO T = 50C

$$\int_{T=25}^{T=50} \frac{dT}{T - T_{\text{wall}}} = -\frac{h \pi D}{\dot{m} c_p} \int_0^L dz$$

$$\ln \left(\frac{T_{\text{out}} - T_{\text{wall}}}{T_{\text{in}} - T_{\text{wall}}} \right) = -\frac{h \pi D L}{\dot{m} c_p}$$

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Logarithmic mean temperature difference

- Log mean temperature difference arises from this differential analysis when both streams are changing temperature

$$LMTD = \frac{\Delta T_A - \Delta T_B}{\ln \left(\frac{\Delta T_A}{\Delta T_B} \right)} = \frac{\Delta T_A - \Delta T_B}{\ln \Delta T_A - \ln \Delta T_B}$$

$$Q = U \times A_r \times LMTD$$

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CORRELATIONS FOR HEAT TRANSFER COEFFICIENT

- As with the "friction factor", we look for the appropriate correlation that uses the correct dimensionless groups.
- For heat transfer we need to find a value for the Nusselt number, Nu , in terms of the Reynolds number, Re , and the Prandtl number, Pr .

$$Nu \equiv \frac{h D}{k} \quad Pr \equiv \frac{\nu}{\alpha} = \frac{\mu c_p}{k} = \frac{\mu c_p}{k}$$

THE APPROPRIATE CORRELATION IS:

$$Nu = 0.023 Re^{0.8} Pr^{0.4}$$

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Imperial Flowsheet

Packed Towers

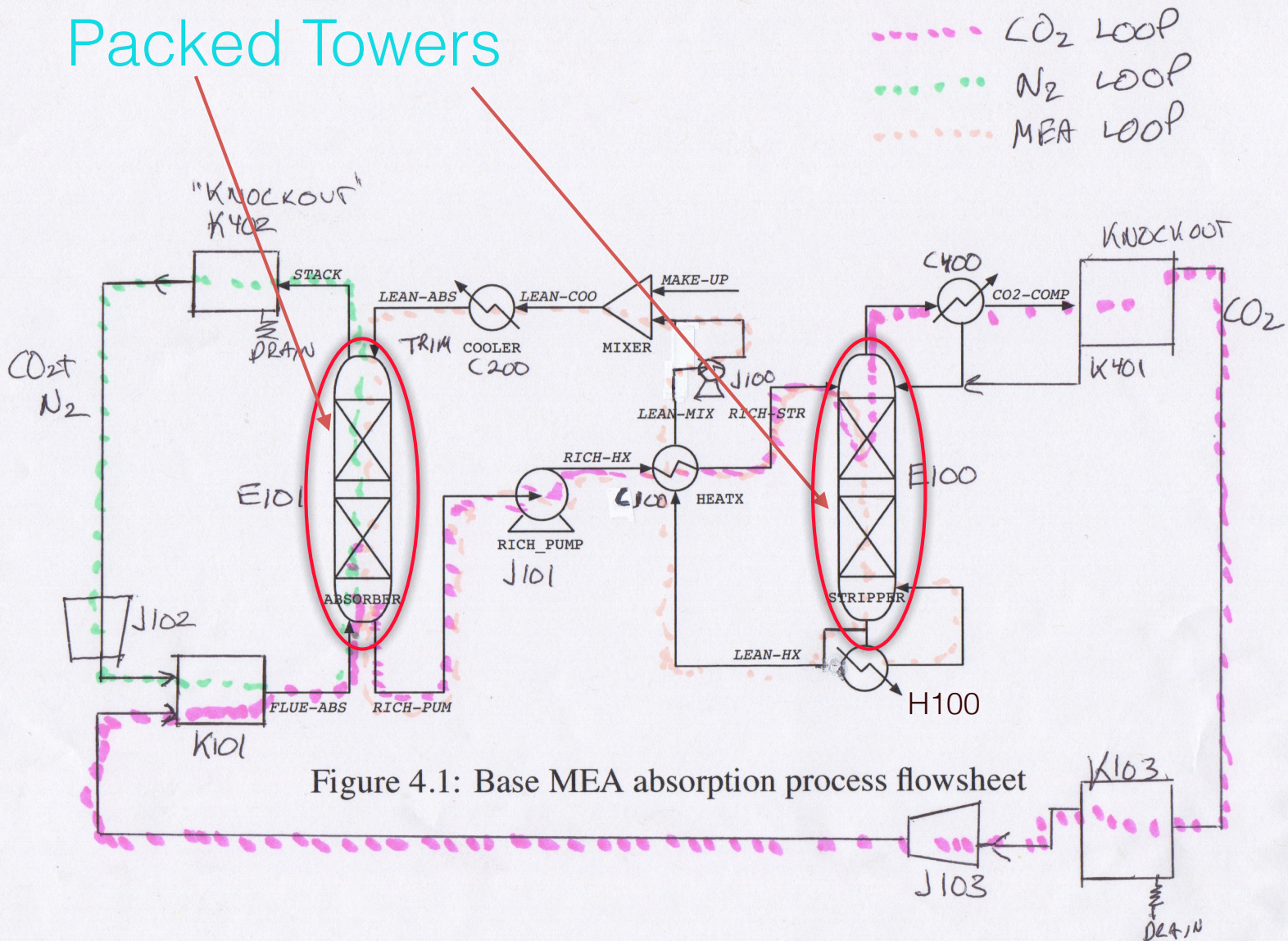
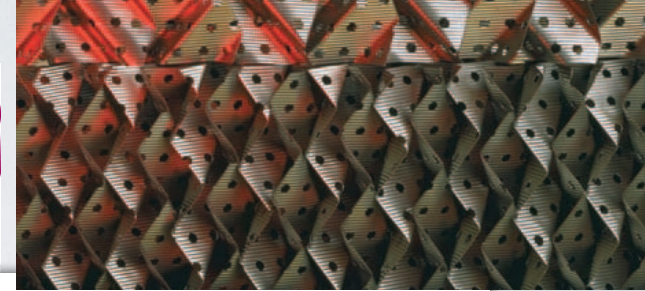
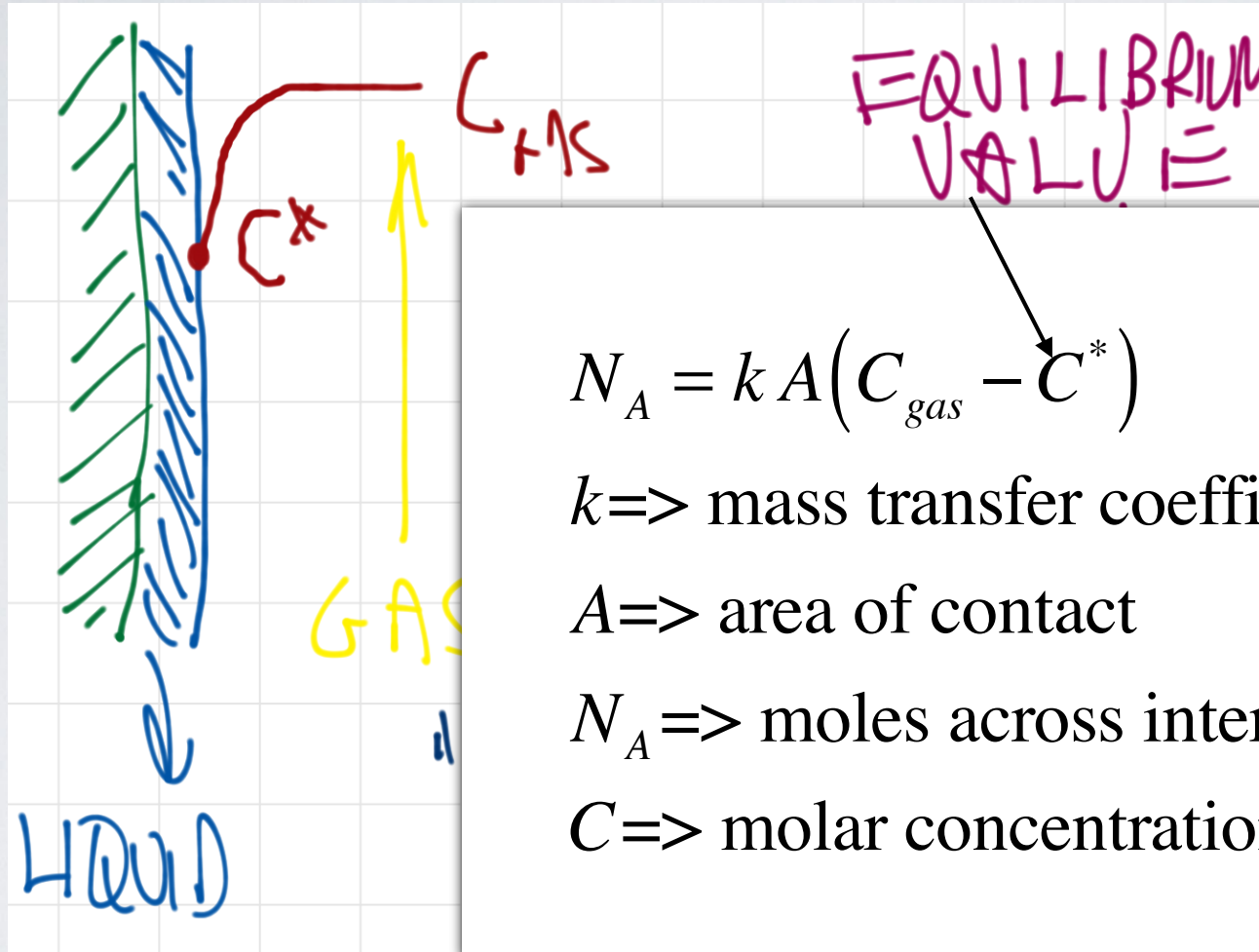


Figure 4.1: Base MEA absorption process flowsheet

EXAMPLE TOPIC: MASS TRANSFER IN MEA PROCESS

- The gas composition can be sampled in the absorber at 6 locations.
- Students need to calculate the local mass transfer coefficient at each location.
 - They compare results to “claims” by the packing manufacturer (which are in height of transfer unit).

MASS TRANSFER RATE EQUATION



$$N_A = k A (C_{gas} - C^*)$$

$k \Rightarrow$ mass transfer coefficient

$A \Rightarrow$ area of contact

$N_A \Rightarrow$ moles across interface/time

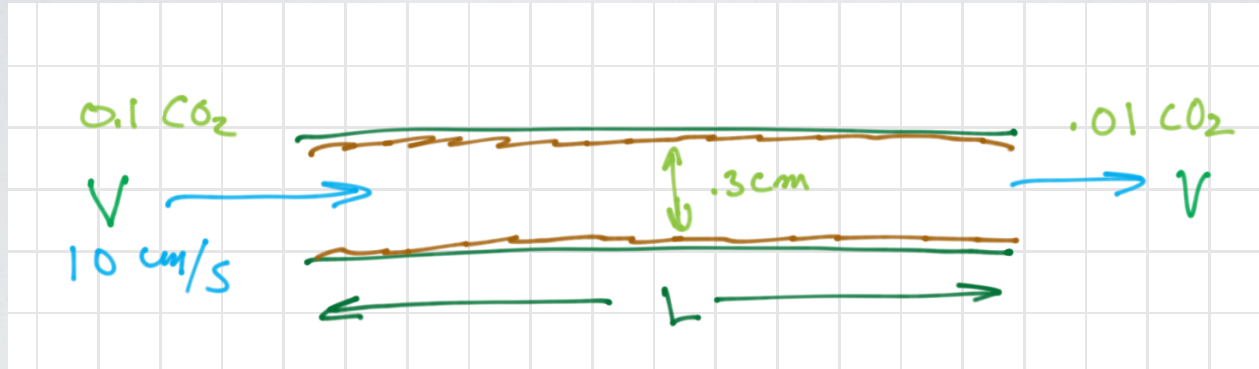
$C \Rightarrow$ molar concentration of CO_2 in gas

Flux = rate coefficient * (linear driving force)

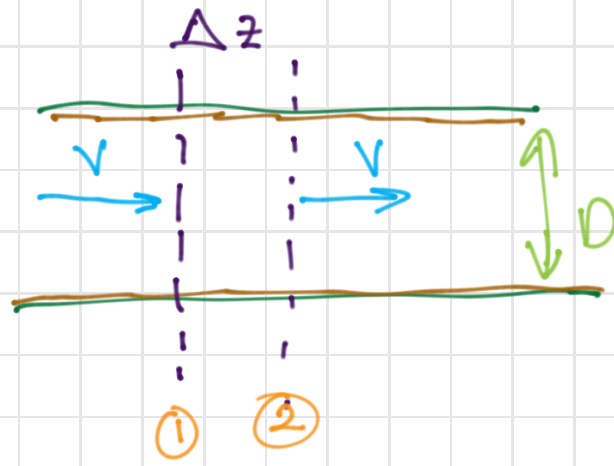
SIMPLEST DIFFERENTIAL MASS TRANSFER PROBLEM

- A Gas mixture that contains CO₂ is flowing in a circular tube. (Could do constant wall T for heat transfer.)
- The wall is made of a CO₂ reactive absorbent.
- Thus, the CO₂ will decrease along the way.
- We need to determine the length of the tube to allow the CO₂ to reach the prescribed final value.

SCHEMATIC



- “monolith” geometry
- CO₂ concentration at wall is kept at 0
- For a given V , what is value of L required?
- To answer this, we need to formulate this as a differential problem.



(MOLES) MASS BALANCE ON A DIFFERENTIAL SLICE OF COLUMN

MOLES OF A CROSSING ① - PER TIME - MOLES OF A CROSSING ② - PER TIME =

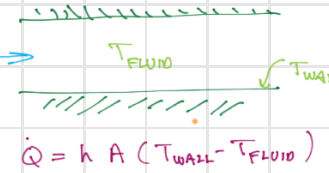
MOLES OF A THAT ADSORB PER TIME

WE NEED! $\frac{n}{V} = \frac{\text{MOLES}}{\text{VOLUME}}$ (IDEAL GAS)

(VOLUMETRIC FLOW $V(\text{AREA})$ \times $\frac{n}{V}$ \times MOLE FRACTION y)

MOLES OF A THAT
ADSORB PER TIME

RECALL:


$$\dot{Q} = h A (T_{WALL} - T_{FLUID})$$

$$N_A A_{WALL} = k \frac{m}{V} (y - y^*) \pi D \Delta z$$

SO OUR MOLE BALANCE ON
DIFFERENTIAL SLICE:

$$\begin{aligned} \frac{\pi D^2}{4} V \frac{m}{V} y \Big|_1 - \frac{\pi D^2}{4} V \frac{m}{V} y \Big|_2 \\ = k \frac{m}{V} (y - y^*) \pi D \Delta z \end{aligned}$$

TAKE LIMIT AS $\Delta z \rightarrow 0$

$$\cancel{\frac{\pi D^2}{4}} V \cancel{\frac{m}{V}} dy = \cancel{k \frac{m}{V}} (y - y^*) \cancel{\pi D} dz$$

SIMPLIFY:

$$\frac{dy}{y - y^*} = \frac{4k}{VD} dz$$

FOR OUR PROBLEM
 $y^* = 0$

WE CAN EASILY INTEGRATE

$$\int_{y_m}^{y_{out}} \frac{dy}{y} = \frac{4k}{VD} \int_0^L dz$$

$$\ln\left(\frac{y_{out}}{y_m}\right) = \frac{4k}{VD} (-L)$$

Length of tube needed: $L = \frac{VD}{4k} \ln\left(\frac{y_m}{y_{out}}\right)$

Exactly
analogous
formulae

For a packed
bed, height of
packing:

$$Z = -\left(\frac{G/A\tau}{ka}\right) \ln\left(\frac{y_1}{y_2}\right)$$

Height of
transfer
unit

Number
of transfer
units

PREP-COURSE LAB EXPERIENCE

- We have students run one thermodynamics experiment (Rankine or Vapor Compression cycle) in our lab at some point in the spring semester
 - This facilitates the schedule at Imperial College.
 - We can “check them out” on the basics of experimental laboratory safety and performance.
 - With these results, they are free to do as much work (data analysis and writing) ahead of time....
- New this year: We will also show them the basic workings of the heat transfer and gas absorber experiments (with them free to video the events.)

SCHEDULE AND STUDENT WORK

- We have one written report due at 5 PM on the 2nd, 3rd and 4th Wednesdays
- The Pilot Plant reports are due on 5th Thursday.
- The oral presentations are on the 6th Wednesday.
- Quality of written reports is essentially as good as those produced in Junior Lab
- The oral reports are better!

WRITTEN REPORTS

- Full length (i.e., 20 pages of text and 5-7 figures + appendices)
- For the Introduction, students must find some connection between the technology of interest and the location of Great Britain or Europe.
- Students are supported by “Program Assistants” (just- graduated seniors) who (are supposed to) know one of the 4 subject areas in extra depth, but all who know well how to divide the work to construct a good report.
- Faculty could be on-site or available by video-con (*Zoom* is great if you are stuck with Adobe!!)
- From both (mjm observations) and focus groups (interviewed by Kerry Meyers, one of our teaching faculty), we think that the highly focused effort over about ~60 hours (Sunday night to Wed afternoon), with support available, seems to be the “trick”.

(MJM POINTS OF EMPHASIS)

- Understand the fundamentals to at least a reasonable degree
- Get the numbers correct!
- Learn to write an informative, clear Abstract
- Discuss the results with coherent, logical arguments supported by the underlying theory.

“CULTURAL ASPECTS”

- Students have 3 of the 5 Fridays (+ all weekends) off for travel
 - They go all over Europe and around GB
- There are three fantastic Museums next to the Imperial Campus (no admission charge) that can visited for short time periods — say during lunch.
 - We have mjm (favorites) slides for every lecture!
- We have been doing 2 “popular” musicals and *The Mousetrap*, usually with a dinner together before, and couple of other evening social events together.
 - A surprising fraction of students have never seen “*Broadway level*” performances before.
 - This is primed in the spring lectures as well!
- Final Day around town to St. Paul’s, Tower Bridge, Borough Market, Tower of London...

SUMMARY

- We have been successful at “teaching” our “Junior” laboratory course and a Unit Operations course, that uses an exquisitely unique pilot plant at Imperial College, to students who are 1 to 1.5 years too “young”
- This has been facilitated by ~complete alignment of the lab and pilot plant onto the unit operations topics of fluid flow, heat and mass transfer and process control.
- Also, there is a high level of faculty and TA support and the students are completely focused on the task at hand for critical time-periods before reports are due.
 - They also benefit from living “together”.
- If there is any interest, a complete set of slides, with practice problems for four, 3-hour sessions done in 2017 for students from Dalian University is available.

LONDON

